Amendments to the Specification:

Please replace the second paragraph (first full paragraph) on page 5 with the following amended paragraph:

In the invention, the hollow fiber membranes are bundled, that is, a plurality of many capillary filtration membranes are collected in parallel, so that fluid simultaneously enters all of the bundled membranes at the same time, and is discharged simultaneously from all the membranes. "Bundled" also suggests that the individual hollow fiber membranes are generally contiguous, as the term "bundle" is used in the '006 Patent to Ohkubo et al. The inlet ends of the plurality of membranes in the preferred embodiment ~~a~~ are generally within a common imaginary plane and their outlet ends also preferably are in or about a second common plane.

Please replace the third paragraph (second full paragraph) on page 5 with the following amended paragraph:

The invention provides a filtering apparatus wherein at least one of the membrane modules is provided with at least one feed-through conduit extending substantially in the longitudinal direction through the membrane module. Depending on the specific circumstances, the option is to use only one or a few membrane modules provided with such feed-through conduit, or to ~~apply~~ supply a filtering system in which all membrane modules are provided with such feed-through conduits. The feed-through conduits must be sufficiently large so that there is little or no flow resistance, and a decline in performance due to pressure reductions is prevented.

Please replace the first paragraph (a full paragraph) on page 7 with the following amended paragraph:

It is seen, however, that the axial flow of fluid through each capillary membrane is unidirectional. Fluid to be filtered enters one end of an individual capillary membrane, and exits the membrane ~~either~~ by osmotic transfer radially outward through the membrane wall, or by passage through the entire length of the fiber membrane. This is in contradistinction to some known devices, which force fluid to be filtered radially inward through the capillary membrane walls, that is, from outside the hollow fiber into its interior. In such devices, however, efficiency may be impaired due to the fact that upon entering the membrane interior, the pressure differences do not clearly dictate the direction of discharge; upon admittance to the membrane interior, the filtered fluid can flow either direction within the tubular membrane, toward either end thereof, until a prevailing pressure bias is obtained. Dominant pressure differentials may not occur until near the ends of the capillary membranes, allowing for impaired flow and eddy currents within the membrane, particularly near the medial portion of its length. In contrast, fluid flowing through the capillary membranes of the inventive apparatus is at all times directed by a pressure bias that directs the fluid into the capillary membrane, and one direction axially along its length. The result is a much more efficient fluid flow, without sacrificing the benefit of exploiting the entire capillary membrane length.

Please replace the second (partial) paragraph on page 7 (continuing to page 8) with the following amended paragraph:

The filtering device illustrated in Fig. 2 comprises a pressure vessel **200** having a feed connection **210** for the liquid to be filtered, formed by one connective point, and a filtrate connection **220** for the filtered liquid (the permeate or filtrate), formed by two connective points. For illustration purposes, the pressure vessel **200** in Fig. 2 comprises two different membrane modules **101**, **102**. However, in practice the number of membrane modules will be larger, as shown in Fig. 1, and the membrane modules will be identical. It is also possible that only one membrane module is used in a pressure vessel. For good positioning of the membrane module **101** inside the pressure vessel **200**, the filter housing **110** of the membrane module **101**

fits closely to the inside wall of the pressure vessel **200**, leaving little or no space between them. Inside the pressure vessel **200**, spacers are used to position the membrane module **102** between the inside wall of the pressure vessel **200** and the filter housing **110**. Inside the filter housing **110**, a membrane compartment **120** comprises a bundle of capillary filtration membranes **121** which, at both ends of the membrane ~~module **100**~~ modules **101, 102**, are cased in membrane holders **130**. In practice, said capillary filtration membranes will usually be micro or ultrafiltration hollow fiber membranes. Further, a permeate discharge compartment **140** and feed-through conduits **150** are provided. The membrane holders **130** close off the space between the capillary filtration membranes **121**, the filter housing **110**, the permeate discharge compartment **140** and the feed-through conduits **150**. In the embodiment shown, the membrane holders **130** are formed from a resin applied in the membrane module, in which resin the capillary filtration membranes **121** are embedded. In the embodiment of the membrane module shown, both ends of all the hollow fiber capillary filtration membranes remain open to receive or discharge fluid from the membranes.

Please replace the last (partial) paragraph on page 8 (continuing on page 9) with the following amended paragraph:

Another advantage is that also the right-hand ~~sides~~ ends of the capillary filtration membranes **121** (as oriented in the figures) of the membrane modules **101, 102** shown in Fig. 2, are supplied with liquid to be filtered. The result is an extremely constant pressure inside the individual capillary filtration membranes **121**, so that the trans-membrane pressure in the longitudinal or axial direction of each individual capillary filtration membrane will decrease a negligible amount. This improves the filtration performance of the particular membrane module. In that case it may be advantageous to provide all membrane modules in a filtering system with feed-through conduits. When considering this option, an optimum must be found between a loss

of membrane surface due to the incorporation of the feed-through conduit, and the elimination of pressure drops due to the addition of said feed-through conduits.